NJWEA 109th Annual Conference Session: Air Pollution & GHG Atlantic City, NJ May 7, 2024

PONCH-H2O - Advanced Wastewater Resource Recovery for Enhanced Carbon Reduction at WRRFs

By: Edward Weinberg, P.E., President, ESSRE Consulting, Inc.



Presentation Outline

- Meet PONCH-H₂O (Phosphorus, Oxygen, Nitrogen, Carbon, Hydrogen for enhanced H₂O & air quality)
- Focus on Carbon Capture & Utilization and Nutrient N-Nitrate Recovery/Reuse as Ammonia for Hydrogen
- GHG CO₂ Biogas Reduction Driven by Microalgae
- PONCH-H₂O Outcomes, Key Takeaways

WRRF CO₂ Capture and Reuse Project C, N & P, O₂, H₂

Mass Cultivation of Microalgae in Photobioreactors – Net Negative C Operations







 $106CO_2 + 16HNO_3 + H_3PO_4 + 78 H_20 \implies C_{106}H_{175}O_{42}N_{16}P + 150O_2$



Carbon Reuse via Microalgae

Biofuels

Biodiesel, Renewable Diesel, and SAF

Bioproducts

- Carotenoids -> Pigments, <u>Nutraceuticals</u>
- Proteins
- Sugars/Starches
- Soil amendment/fertilizer <u>Biochar</u>



CO₂ Emissions Sources

- Raw Biogas/Landfill Gas Feedstock 35% 65% CO₂
- Biogas CHP 8% 12% CO₂
- Biogas/NG Industrial Steam Boiler 5% 6% CO₂
- Biogas Sludge Drying 8% 10% CO₂
- Purified Biogas RNG 97% 99% CO₂
- Solar Sludge Drying 400 ppm 1000 ppm CO₂

Waste Heat Recovery

Optimum Algae Cultivation = ~85° F; Engine Exhaust = ~1000° F



- Three Choices of WHRUs
 - ORC (Electric Power)
 - Waste Heat Chiller (Cooling)
 Gas Cooling or Chilled Water
 - Waste Heat Boiler (Heating)

Offset LED Lighting

Drying or Pyrolysis of Wet Algae

Algal System Technology/Flue Gas Conditioning



FLUE GAS

Flue gas is captured using a slipstream and cooled using Waste Heat Recovery Units (not shown)



FLUE GAS FILTRATION

A simple H₂O quench trap cools the water to 85F and traps any particulates



FLUE GAS COMPRESSION

Flue gas is fed to a
Liquid Ring Compressor
to minimize heat of
compression. The water
is separated from the
flue gas which is then
directed to the
photobioreactors (PBRs)



WATER CONDITION

Compressor recirculating water is neutralized to pH 7, nutrient and makeup water added and cooled to <70F for re-use through the compressor.

Microalgae Cultivation Technology/Process



FLUE GAS INJECTION

A special gas sparger was developed inhouse to ensure rapid transfer of gas chemistry to the culture using microbubbles that increase light penetration and enhance tall column mixing throughout





GROWTH ENHANCEMENT

Advanced LED lighting technology developed in-house to enhance growth and nutritional value of the algae via proprietary lighting strategies that "photo-stress" the algae and reduce energy consumption



CULTURE HARVEST

When the algae gets too dense for light penetration, the automation drains 10% of the tank to thin out the culture to get more light



CULTURE HOLDING

Harvested algae is centrifuged (not shown) to concentrate the algae into paste product for conversion. Centrate is recirculated to the PBRs.

Why Algae? - Host of Bioproducts













- Algae and algae oil is used in the following products (partial list)
 - Nutraceutical products, eye nutrients, Omega-3 Fatty Acids
 - Skin conditioners
 - Cosmetic and paint thickeners





- Animal and numan food supplements PROTEINS
 - The HY-TEK Bio algae s.HTB-1 can bring as much as \$40/lb from an algae brokerage house
- 90-95% Oxygen from photosynthesis is a reusable marketable commodity
- Direct replacement for Palm Oil
- **Biochar Soil Amendment**



THE BUSINESS PLAN





PONCH-H2O Facilities

ONCE THE INVESTOR IS PAID BACK, THE PONCH-H₂O FACILITY IS TURNED OVER TO THE CLIENT AT NO COST ALONG WITH % OF THE REVENUE STREAM FROM THE SALE OF THE ALGAE TO PAY FOR O&M PLUS CONTINUED REVENUE STREAMS THAT MAXIMIZE RETURN and ENABLE MULTIPLE COMMUNITY BENEFITS

10-Year Algae Production & Financial Projections

- EXAMPLE: Containerized Algae Facility Adjacent to Biogas Engine Room
- PRODUCTION: 1149Tons Algae p.a.
- DETAILS: 10 PBRs; Capital Initial Investment \$4.375M; Breakeven Payback by Yr. 3 of operation; Total 10-Yr Revenue ~ \$39M

NPV ~\$6.25M; IRR% 40.7

- INVESTOR OUTCOME: If 15% of Capital Cost, Investor net profit ~\$2.8M
- CLIMATE OUTCOME: Total Carbon Dioxide Removed, 2095 Tons, p.a.

Note: Assume a system availability factor of 75% during year one, otherwise 90% availability factor

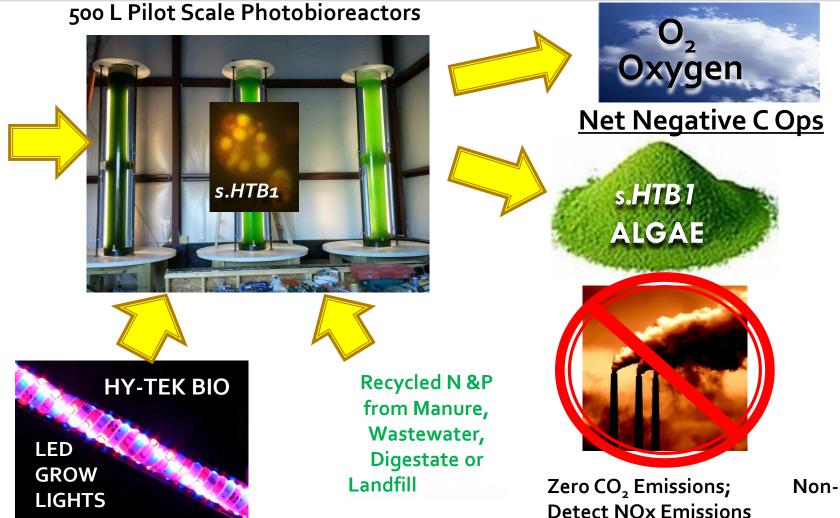
PONCH-H2O PROJECT ORGANIZATIONAL STRUCTURE

Commercial Demonstration Project (Alpha, Beta, etc.) Structure Overview DOE, State & RD & D Academic Debt **Equity Local Grants** Investment Funds or Funding Project Company (LF or WWRF JV, LLC) Operations & Maintenance Long Term Services Research & DEI Consortium **Execution Consortium** LF or WWRF Owner/Operator · Owner Operator · DOE, USDA, EPA, NSF, A/E or GC ESSRE & HY-TEK BIO Others 3rd Party O&M Universities Fluor A/E HY-TEK BIO HY-TEK BIO · Non-Profit Community DEI ESSRE • Owner/Operator's GC ESSRE • Owner/Operator (if Investor) 3rd Party O&M Provider

PONCH-H₂O Review

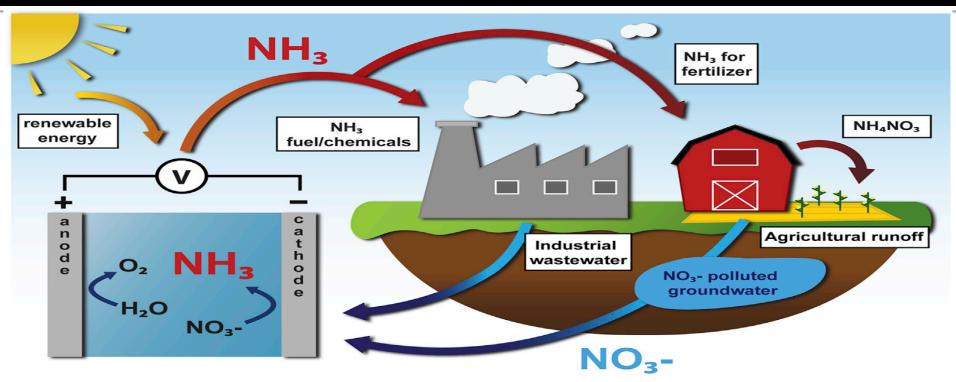


Digesters/Landfills
Biogas Engine Exhaust
LFG Engine Exhaust
RNG Waste CO₂ Tail Gas



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ONE WATER Goal: Nitrate Polluted Water/Wastewater Closed-loop Transformation into Reuseable Ammonia Based Products

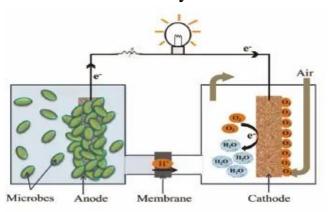


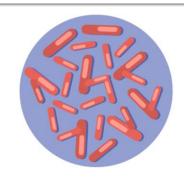
Electrochemical membrane treatment alternative to denitrification or Nitrate selective Ion Exchange processes, which respectively transforms pollutant nutrient N ammonia gas or liquid ammonium salt fertilizer solution. The built environment N cycle image shows two distinct opportunities: 1) Concentrated nitrate wastewater from industry and 2) Dilute nitrate waters from farm runoff or drainage and treated POTW effluent (not shown)

N-Nitrate Removal "Pain Points"



Cons: Frequent regeneration
Nitrate is only concentrated and
then T&D'ed Costly Brine
Waste Disposal; No resource
recovery





Biological Denitrification

Cons: Long hydraulic retention times. Additional carbon source. No resource recovery – inert N_2 gas emitted

Bio-Electrochemical Systems (BES)

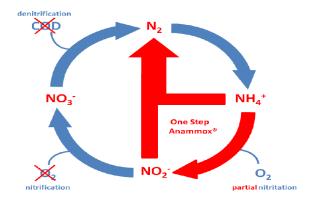
Cons: Several Hybrid cases (MFC, MEC) in development with removal of COD and production of energy as the primary outcomes

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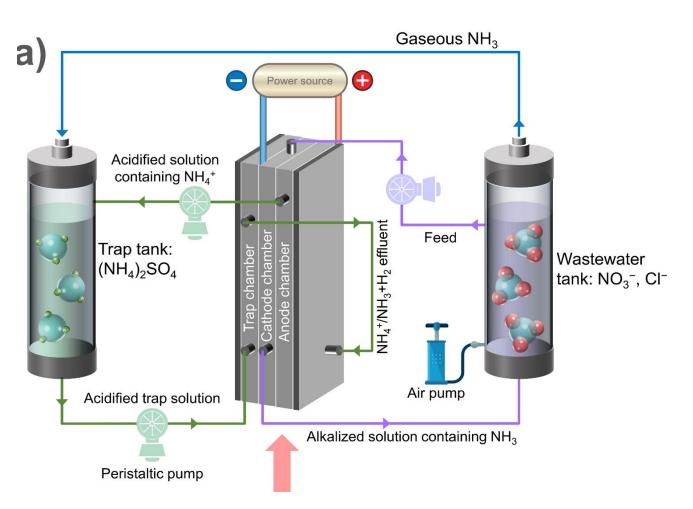
Physical Membrane Separation

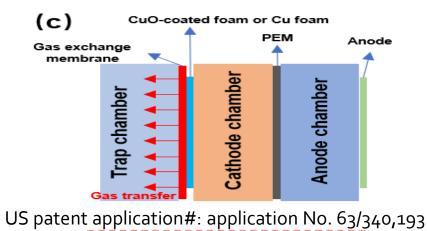
Cons: Prone to fouling, frequent cleaning; Concentrate Disposal; Energy intensive; High Capex cost; no resource recovery

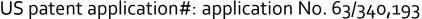


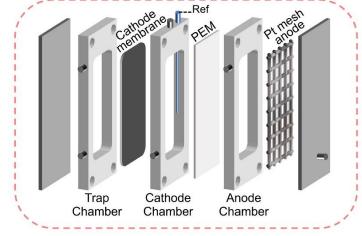
Partial Denitrification Anammox; SND; Alternative C Sources

Schematics of an ElectroChemical Membrane (ECM) Cell and System







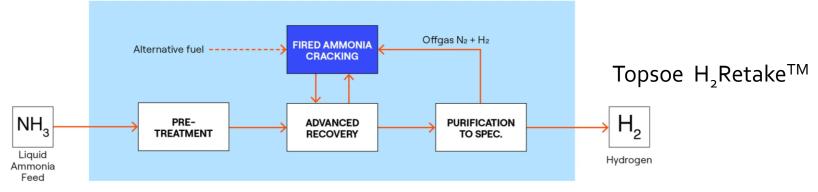


Ammonia "Cracking" for Hydrogen



Ammonia is emerging as a clear front runner for transporting Hydrogen because it has a much higher density and the gas can be readily liquefied at room temperature and low pressure for high

volume, safer transport.



Once delivered to the H2 use site, the ammonia is "cracked" (decomposed) to release the H2 gas. It can then be used as a zero Carbon fuel or as a raw material in industrial processes (e.g., oil refineries).

Ammonia vs. H2 vs. Battery Storage

Energy storage comparison



30,000 gallon underground tank contains 200 MWh (plus 600 MMBTU CHP heat

Capital cost ~\$100K



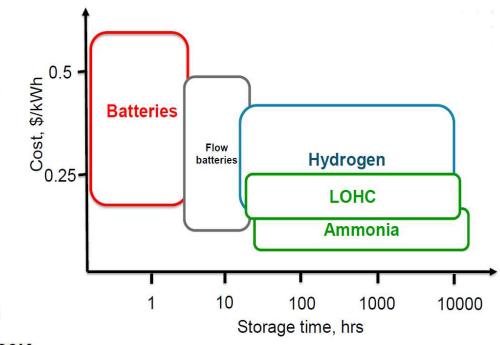
204 MWh NGK battery in Japan

or

40 x

5 MWh A123 battery in Chile

Levelized cost of energy storage

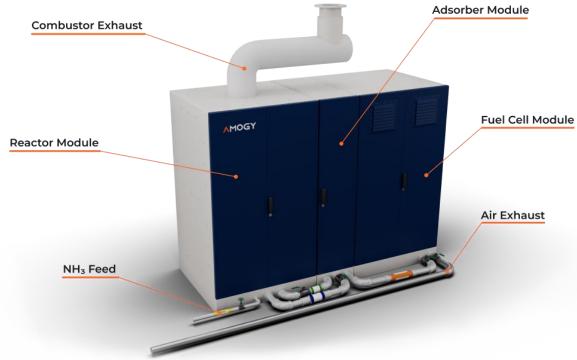


Capital cost \$50,000 - 100,000K

Source: Soloveichik, NH₃ Fuel Conference 2016

Ammonia to Power

Amogy Ammonia Fuel Cell



Zero-C power replaces polluting diesel generators for backup power at **WRRFs**



Zero-C power for cargo & heavy duty handling equipment, maritime vessels, EV charging stations, and data centers



Key Take Aways

- PONCH-H2O = WRRF & Industrial Decarbonization
 - Complete CO2 removal from Biogas, LFG Utilization while maximizing returns
 - Net Negative Carbon, O2 reuse, and Novel Nitrate Transformation to Ammonium Salt Nutrients for Microalgae or Ammonia/H2 for fuel at WRRFs and elsewhere
- Regenerative Ag Carbon Markets
 - PONCH-H2O: Transfers Atmospheric CO2 and Sequesters C as Biochar onto Soil for Maximum Dual Impact on Climate Change
- Net Zero GHG Emissions
 - ESG Scope 1, 2 or 3 Emissions wherever fossil fuel is combusted

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Questions





